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# Scale-fragment formation impairing geothermal energy production: interacting H<sub>2</sub>S corrosion and CaCO<sub>3</sub> crystal growth

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## Abstract

**Background:** Mineral precipitates (scaling) from deep saline thermal waters often constitute a major problem during geothermal energy production. The occurrence of scale-fragments accumulating and clogging pipes, filters, and heat exchangers is of particular concern regarding an efficient energy extraction.

Methods: Carbonate scale-fragments from different sections of two geothermal power plants were collected and studied in a high-resolution scaling forensic approach comprising of microstructural characterization, elemental mapping, and stable carbon and oxygen isotope transects. The solid-phase analyses were evaluated in the context of natural environmental and technical (man-made) production conditions.

**Results and discussion:** Our results indicate an interaction of metal sulfide mineral layers mainly from H<sub>2</sub>S corrosion of the steel pipes and CaCO<sub>3</sub> nucleation and crystal growth. A conceptual model of scale-fragment development addresses the relevance of two key interfaces: 1) the corrosion layer between the steel substrate and calcite scale and 2) the scale surface versus thermal fluid flow. The corrosion products constitute an attractive crystallization substrate of brittle and mechanically weak consistency. A rough carbonate scale surface tends to induce (micro) turbulences and increased flow resistance (frictional forces). These factors promote partial exfoliation, scale-fragment mobilization, and rapid clogging. This investigation highlights the potential of detailed petrographic and geochemical analyses of mineral precipitates for evaluating favorable versus unfavorable processes in geotechnical environmental settings.

Keywords: Scaling, Mineral precipitates, Calcite, Sulfide corrosion, Steel corrosion, Geothermal energy, Heat exchanger, Fluid–solid interaction

## Background

Geothermal power gains in importance for heat and electricity production owing to its base-load capabilities compared to other renewable energy sources and promising technological developments (DiPippo 2015; Finster et al. 2015). Many geothermal installations (e.g., hydrothermal doublet systems), however, face major operational challenges, such as unwanted scaling (mineral precipitation) and corrosion of components accompanying the exploitation of typically high salinity, temperature, and gas content thermal waters from deep wells (Mundhenk et al. 2013; Klapper et al. 2016). The extent and



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site-specific characteristics of scaling and corrosion problems depend on geogenic as well as man-made environmental conditions, i.e., hydrogeochemistry and geology, water reservoir depth (temperature/pressure), flow rate, operating pressure, geometries, and composition of materials of the geothermal facilities.

Variable environmental (production) conditions and disturbed natural hydrogeochemical equilibria (temperature/pressure changes, CO<sub>2</sub>/H<sub>2</sub>O outgassing) can significantly promote scaling in production wells, downhole pumps, transport pipes, valves, and heat exchangers leading to inner diameter reduction, disturbed flow regimes, and clogging counteracting efficient energy extraction (Zarrouk et al. 2014). Similarly, mineral precipitation and mobilization (e.g., fine particles) can significantly reduce the reinjection efficiency of cooled thermal fluids depending on the respective physicochemical injection conditions, aquifer lithology, and hydraulic parameters (Rivera Diaz et al. 2016). Calcium carbonate  $(CaCO_3)$  precipitation is widespread in low- to moderate enthalpy geothermal facilities tapping deep limestone/dolomite aquifers (e.g., Central European sedimentary basins) entailing elevated dissolved carbonate and carbon dioxide concentrations (Alt-Epping et al. 2013; Stober 2014). Silica/silicates, in contrast, dominate scale formation in high-enthalpy geothermal regions (e.g., Iceland, New Zealand; Gunnarsson and Arnórsson 2005; Zarrouk et al. 2014). Sulfates, sulfides, (hydro)oxides, or even chlorides can also form scale deposits (Corsi 1986; Regenspurg et al. 2015). Next to problematic mineral precipitation, corrosion of varying chemistry and degree can significantly harm carbon- and low-alloy steel components as well as concrete casings of geothermal installations (Mundhenk et al. 2013; Nogara and Zarrouk 2014). These material deterioration processes mostly depend on the prevailing electrochemical (redox) conditions and critical solution/gas constituents of the thermal fluid. Reducing conditions in aquifers and geothermal wells typically result in H<sub>2</sub>S-based corrosion and formation of various metal sulfides, while (intermittent) oxidizing conditions support the occurrence of iron-(oxy) hydroxides (Valdez et al. 2009; Bai et al. 2014). Steel corrosion and scaling processes may further be affected (e.g., catalyzed) by diverse microbial communities, i.e., playing an active (e.g., changing hydrochemistry) or passive (e.g., being a substrate) role for corrosion/scale mineral crystallization (Lanneluc et al. 2015; Würdemann et al. 2016).

The occurrence of scale-fragments (flakes) of variable dimensions constitutes a particular development of scaling in geothermal installations (Wolfgramm et al. 2011; Bauer et al. 2014). Typically thin (mm-range) scale deposits form in wells and transport pipes and are later mobilized (flaked off) in the course of thermal water flow. The growth and subsequent mobilization of such scale-fragments can cause specific and often serious problems, i.e., material damages and a rapid deterioration in the efficiency of hydrogeothermal heat extraction. Over short time intervals (e.g., weeks to few months in this study), critical accumulation, cementation, and clogging of filters and heat exchangers can occur. This leads to significantly reduced fluid flows and energy transfers. As a consequence, necessary maintenance intervals are shortened and impaired technical components (e.g., plate or tube bundle heat exchangers) have to be replaced unscheduled. In worst cases, the commercial viability of the geothermal infrastructure becomes a subject of debate.

In this study, we have conducted a scaling forensic approach. The scale-fragments themselves constitute a valuable chemical archive, i.e., their variable chemical composition and particular fabric (crystal growth) capture production-specific fluid–solid

interaction. Applying high-resolution analytical techniques, the natural and man-made environmental conditions promoting unwanted carbonate scaling, corrosion, and fragmentation are evaluated comparable to scientific approaches in paleoenvironmental (paleoclimate) studies based on mineral precipitates (e.g., Boch et al. 2011; Dietzel et al. 2015). An increased process understanding of the particular carbonate scale growth dynamics and scale-fragment formation is targeted, i.e., elucidating the favorable versus unfavorable environmental and technical conditions that support scale-fragment evolution.

## Sites, samples, and methods

Mineral precipitates (scales) were collected from different sections of two geothermal power plants nearly identical in construction (henceforward referred to as KIR and DUR), suffering from major problems with scale-fragment formation, i.e., the mobilization and accumulation of scale material formed inside pipes and subsequently clogging the outer faces of heat exchangers. Located in southern Germany, the two hydrogeothermal doublet systems with Organic Rankine Cycles produce district heat and electric power (7 MW<sub>el</sub> max. each; ~31 GWh/a; Weber et al. 2016) from deep thermal water production and reinjection wells (KIR: GT1 4214 m, GT2 4452 m final measured depth; DUR: GT1 4393 m, GT2a 4530 m) tapping the regional Malm (Upper Jurassic) limestone/dolomite aquifer overlain by Cretaceous marls and sandstones followed by Paleogene to Late Miocene successions of marls, sands, and clays (Mayrhofer et al. 2014; Dussel et al. 2016; Goldbrunner and Vasvari 2016). Top of Malm at the location KIR is reached at 3447 m (GT1) and 3711 m (GT2) and at 3715 and 3641 m for GT1 and GT2a at DUR, respectively. The corresponding open hole sections range from 650 to 930 m. The thermal fluid temperatures reach 134 and 136 °C at the wellheads and maximum discharges are 135 and 115 l/s for KIR and DUR, respectively. Scale-fragment samples were recovered from dismounted well steel pipes of different depths (increasing sample numbers, e.g., 1-81) and from the outer (water inlet) sides of (tube bundle) heat exchangers in the plants (samples "WT") during a major maintenance procedure of both facilities in September 2014 (Fig. 1). Individual up to 10-cm-long and typically a few millimeters thick fragments (flakes) were sampled from the interior surfaces of the conventional (low-alloy) steel pipes (Fig. 1b, d) afore being mounted vertically in different borehole depths. Accumulations of cemented scale-fragments were also sampled as impressive blocks of dm-size heavily blocking the outer heat exchanger surfaces (Fig. 1c, e). Scale-fragments recurrently assembling such massive blocks over time (typically within weeks to months), however, were deposited and mobilized within a relatively short spatial distance, i.e., they originate from a thermal water transport section after some upstream filter equipment of the uppermost production well water flow. After impacting and accumulation on the outer heat exchanger surface, the scale-fragments were successively cemented and compacted by ongoing mineral precipitation from the streaming thermal water.

Selected and representative scale-fragment samples from both study sites were investigated in detail via state-of-the-art mineralogical and geochemical methods. Solidphase characterization included powder X-ray diffraction (XRD) using a PANalytical X'Pert PRO diffractometer equipped with a Co-K $\alpha$  X-ray radiation source (40 mA,



40 kV) and an X'Celerator detector and applying measurement parameters 4°–85° 2 $\theta$  range, ~0.01° step propagation (2 $\theta$ ), and 40 s/step counting time. Typical sample aliquots amounted to 0.5 g of powder pestled for bulk (carbonate) scale analyses and ca. 0.1 g for identifying the insoluble residuum after dissolving the (carbonate) scale matrix (ca. 10 g sample) in diluted nitric acid (12 vol.%, for 24 h). Elemental compositions of the scale-fragments were determined with a Philips PW 2404 X-ray fluorescence spectrometer (WDX-XRF) analyzing ca. 0.8 g sample aliquot in fused Li<sub>2</sub>B<sub>4</sub>O<sub>7</sub> glass pellets for the major and minor elements (analytical error 0.5–5 wt.%) and ca. 12 g sample aliquot in pressed powder pellets for the trace elemental compositions (analytical

error <10 wt.%). Loss-on-ignition (L.O.I.) was determined at 1050 °C. Chemical compositions were further analyzed by wet chemistry techniques. Parts of the scale-fragments were powdered and digested with HNO<sub>3</sub> (supra-pure). Measurements of the elements were performed by optical emission spectrometry (ICP-OES, Perkin Elmer Optima 7300DV) and inductively coupled plasma mass spectrometry (ICP-MS, Perkin Elmer Sciex ELAN 6100). Total organic carbon (TOC) was measured with a Carlo-Erba EA11008 Elemental Analyzer. Microscopic (petrographic) characterization of scale samples was conducted based on polished, non-covered thin sections for transmitted and reflected light microscopy (Leica DMLP) connected to an Olympus DP26 camera. Scanning electron microscopy (SEM) was performed on carbon-coated samples using a Zeiss DSM 982 Gemini SEM operated at 2 kV.

Selected scale-fragments were further investigated by high spatial (temporal) resolution analytical techniques involving elemental mapping using the wavelength-dispersive analytical mode (WDX) and back-scattered electron imaging (BSE) using a JEOL JXA-8200 electron microprobe (EPMA). Semi-quantitative elemental distribution images of Ca, Mg, Fe, S, and Si were recorded with an accelerating voltage of 15 kV, a beam current of 30 nA, and  $\sim 1 \,\mu\text{m}$  electron beam resolution. 1000  $\times$  800 point analyses, a step size of 0.44 µm, and a counting time of 15 ms/step yielded elemental distribution maps of  $440 \times 350 \,\mu\text{m}$ . Scale-fragments were also embedded in epoxy resin, cut, and polished to obtain a few millimeters thick cross-sections. Tiny sample amounts (0.25–0.60 mg) were extracted from two selected and embedded scale-fragments at 100 µm spatial resolution (KIR33: 39 samples; DUR34: 10 samples) using an ESI New Wave Research computercontrolled micromill and continuous sampling transects (Spötl and Mattey 2006; Boch et al. 2011). Additional samples from other fragments were recovered using a dentist drill. The stable carbon and oxygen isotopic compositions of the micromilled and drilled carbonate powders were subsequently measured by continuous-flow isotope ratio mass spectrometry (CF-IR-MS), i.e., a Thermo Fisher Scientific GasBench II connected to a Finnigan Delta<sup>plus</sup> XP mass spectrometer, following the procedure reported in Dietzel et al. (2015). Measured isotope ratios are quoted relative to the VPDB standard and typical precision (2 $\sigma$ ) is  $\pm 0.08$  and  $\pm 0.1\%$  for  $\delta^{13}$ C and  $\delta^{18}$ O values, respectively. In order to discuss fluid (thermal water/gases) versus solid (scale/corrosion) interaction, hydrochemical data from available reports of the two geothermal facilities were used. Mineral saturation states (SI values defined as ion activity product versus solubility product on a logarithmic scale, i.e.,  $SI = \log [IAP/K_{sp}]$ , SI = 0 means saturation) and aqueous solution CO<sub>2</sub> partial pressures were calculated based on these data applying the PHREEQC computer code for hydrogeochemical modeling (version 3.2.0, phreeqc.dat database, Parkhurst and Appelo 2013).

## **Results and discussion**

## Scale chemistry and fabric

Several scale-fragments of 2–10 cm size and 1–4 mm thickness were analyzed for their mineralogical and chemical composition. Our results showed that all of these samples deposited either on the outer side (thermal water influx and obstacle for scale-fragments) of the heat exchangers (e.g., KIR-WT, DUR-WT), at the top (e.g., KIR-GOK), or base (DUR1, KIR1) of the uppermost steel pipe in the borehole and thus close to the

wellhead, or several hundred meters (<1000 m) deep in the borehole (KIR56, DUR81) are almost exclusively composed of Mg-calcite (~90 to 99 wt.%), i.e., crystalline CaCO<sub>3</sub> solid solutions with 5–8 mol-% MgCO<sub>3</sub> (Fig. 2). All of the scale-fragments analyzed revealed a very similar mineralogical and chemical composition. Acid digestion of the prominently dark-colored carbonate scales resulted in a black residuum (insoluble portion) composed of variable contents of metal sulfides and silica (Fig. 3). The sulfides are dominated by FeS (e.g., pyrrhotite, typically <2 wt.% in the scale), CuFeS<sub>2</sub> (chalcopyrite, <1 wt. %), ZnS (sphalerite, <0.5 wt.%), and NiS (millerite, <0.1 wt.%; Fig. 3; Table 1, Additional file 1:





The *black residua* are mainly composed of variable metal sulfide and silica contents of variable crystallinity, i.e., FeS (pyrrhotite), CuFeS<sub>2</sub> (chalcopyrite), ZnS (sphalerite), NiS (millerite), and a SiO<sub>2</sub> component (quartz or adsorbed silica). Minor contents of  $Fe_3O_4$  (magnetite) might result from partial later stage oxidation of iron sulfide

| Sample_ID                      | KIR1   | KIR-GOK | KIR-WT | DUR1   | DUR81  | DUR-WT |
|--------------------------------|--------|---------|--------|--------|--------|--------|
| Component                      | [wt%]  |         |        |        |        |        |
| L.O.I.                         | 45.88  | 43.43   | 43.97  | 43.26  | 43.12  | 43.74  |
| MgO                            | 2.23   | 2.63    | 2.51   | 2.25   | 2.82   | 2.59   |
| Al <sub>2</sub> O <sub>3</sub> | 0.47   | b.d.l.  | b.d.l. | 0.20   | 0.15   | b.d.l. |
| SiO <sub>2</sub>               | 0.56   | 0.08    | 0.04   | 0.13   | 0.11   | 0.06   |
| $P_2O_5$                       | 0.01   | b.d.l.  | 0.03   | 0.01   | 0.01   | b.d.l. |
| SO3                            | 1.84   | 0.65    | 0.35   | 2.40   | 1.07   | 1.03   |
| CaO                            | 46.21  | 52.03   | 52.5   | 49.27  | 51.16  | 51.41  |
| MnO                            | b.d.l. | b.d.l.  | b.d.l. | 0.03   | b.d.l. | b.d.l. |
| Fe <sub>2</sub> O <sub>3</sub> | 2.27   | 1.08    | 0.48   | 2.02   | 1.44   | 0.92   |
| Ni                             | 0.02   | b.d.l.  | b.d.l. | b.d.l. | b.d.l. | b.d.l. |
| Cu                             | 0.18   | b.d.l.  | 0.02   | 0.30   | 0.02   | 0.12   |
| Zn                             | 0.25   | b.d.l.  | b.d.l. | 0.04   | b.d.l. | 0.02   |
| Sr                             | 0.07   | 0.09    | 0.09   | 0.08   | 0.09   | 0.09   |

Table 1 Major and minor elemental composition and loss-on-ignition of selected scalefragments based on X-ray fluorescence (XRF) of fused glass pellets (b.d.l. = below detection limit)

Tables S1, S2). The SiO<sub>2</sub> component (typically <1 wt%) represents quartz (cf. XRD peak in Fig. 2) and also adsorbed amorphous silica. In addition, elevated TOC concentrations of the scale material (up to ~4 wt.%) were measured. The observation of magnetic particles as part of the dark residuum supports significant contributions of pyrrhotite (Fe<sub>1-</sub> <sub>x</sub>S). Minor contents of Fe<sub>3</sub>O<sub>4</sub> (magnetite; Fig. 3) in one sample might result from partial later stage oxidation of iron sulfide. The prominent occurrence of various metal sulfides reflects reducing redox conditions of the scale precipitating thermal waters. The dark color of the otherwise whitish carbonate scales likely originates from the organic content as well as typically dark-colored and finely disseminated metal sulfide particles. The latter is somewhat analogous to hydrothermal "black smoker" deposits of the deep ocean floors (Baker et al. 2016).

Detailed optical characterization of the scale material provided further insights into petrographic and genetic aspects. Macroscopically, the carbonate scales expose welldeveloped crystal faces on their growth surfaces supporting some prominent light reflection (brilliance) in spite of their dark coloring (Fig. 1d). The sparitic fabric entails an extra rough scale surface shaped by numerous individual crystal tips. Microscopic techniques (Fig. 4; Additional file 1: Figure S1) revealed a compact growth fabric with little intra- and intercrystalline porosity of these CaCO<sub>3</sub> precipitates. The crystal shapes display idiomorphic (euhedral), rhombohedral calcite crystals frequently terminating as distinct crystal tips at the actual growth surface, i.e., the interface toward the thermal fluid (Fig. 4a, b, e). Abundant nucleation represented by numerous small crystallites gradually develops toward relatively large (mm-size), columnar Mg-calcite crystals showing rather smooth crystal (grain) boundaries (Fig. 4c, d, f). Such competitive crystal growth after numerous initial crystallites results in the dense interrelation of the scale assembling crystals (Frisia et al. 2000). Importantly, these petrographic and growth characteristics support a brittle consistency of the calcite scale material. Visible light and electron microscopy show the occurrence of various metal sulfides (variable shapes and colors) arranged (i) in distinct layers of alternating thickness at the interface between calcite scale and the underlying (steel) substrate (Fig. 4a, c) and (ii) as recurrent, typically much thinner sulfide layers within the compact carbonate scales (Fig. 4f; Additional file 1: Figure S1C). The omnipresent metal sulfide layers at the scale base most likely are of an in-situ chemical origin, i.e., from an early mineral-forming reaction of the corrosive thermal fluid at the exposed fresh steel surface. This is supported by some overall growth orientation of the sulfide minerals. In contrast, the thin layers within the



Fig. 4 Microscopic characterization of the carbonate scale-fragment fabric. **a** Reflected light (RL) crosssection showing a basal sulfide corrosion layer (*red arrows*), columnar Mg-calcite crystals, and rhombohedral crystal tips forming a rough scale growth surface (*blue arrows*). **b** RL image showing a layer of detrital particles (variable thickness, *yellow arrows*) on the former calcite growth surface (*blue arrow*) and subsequent re-nucleation of numerous calcite crystallites (*white arrows*). **c** Typical metal sulfide layer of variable thickness at the scale-fragment base (*red arrow*). **d** Transmitted light (TL) image of basal corrosion layer being an attractive substrate for abundant calcite nucleation and ongoing competitive crystal growth. **e** Scanning electron microscope (SEM) image of rough scale growth surface showing a dense fabric of rhombohedral calcite crystals. **f** Back-scattered electron (BSE) image illustrating typical metal sulfide layers at the scale-fragment base (partially fractured, *red arrow*) and as thin layers within the compact carbonate scales (*yellow arrows*)

scales possess a more particular (individual grains) character and also strongly variable thicknesses (Fig. 4b; Additional file 1: Figure S1C). This suggests a detrital origin for this type of sulfide layers, i.e., an event-like accumulation after transport in suspension. An important feature consists in the pronounced nucleation of  $CaCO_3$  on the basal sulfide layers (Fig. 4c, d) as well as re-nucleation on later stage (detrital) layers (Fig. 4b).

### Carbonate scaling versus corrosion

Our mineralogical and petrographic results suggest an intimate connection at the basal sulfide layer and calcite scale interface. High spatial resolution electron microprobe elemental maps measured in this study (Fig. 5) support the results from bulk scale chemical analysis, i.e., the layers at the scale base toward the underlying steel pipe substrate primarily consist of Fe-sulfide minerals and some associated SiO<sub>2</sub>. Variable iron and sulfur concentrations in these basal layers represent a gradual development from more or less pure Fe (steel) toward metal sulfides of varying stoichiometric composition. Minor later stage alteration of the sulfides (e.g., oxidation toward goethite, magnetite) might also have occurred according to the microprobe (Fig. 5) and XRD (Fig. 3) results. Regarding the basal layer chemistry and texture, the analyses suggest an origin primarily from H<sub>2</sub>S steel corrosion (Choi et al. 2011; Bai et al. 2014), e.g., represented by the overall chemical reactions:

$$H_2S_{(aq)} = HS^- + H^+$$
(1a)

$$HS^{-} = S^{2-} + H^{+}$$
(1b)

$$Fe_{(s)} + 2H^{+} = Fe^{2+} + H_{2(g)}$$
(1c)

$$Fe_{(s)} = Fe^{2+} + 2e^{-}$$
 (1d)

$$H_2S_{(aq)} + 2e^- = S^{2-} + H_{2(g)}$$
(1e)

$$Fe^{2+} + HS^{-} = FeS + H^{+}$$
<sup>(1f)</sup>

$$Fe_{(s)} + H_2S_{(aq)} = FeS + H_{2(g)}.$$
(1)

Natural (hydrochemistry) as well as technical (conventional low-alloy steel pipes) environmental conditions support a high corrosion potential at both geothermal facilities. Hydrochemical data from the local limestone/dolomite aquifer and production wells of the geothermal installations (Eichinger 2010; Seibt 2010; Wolfgramm et al. 2011; Mayrhofer et al. 2014; Stober 2014; Goldbrunner and Vasvari 2016) reveal strongly reducing redox conditions (up to -360 mV) at pH  $\sim$ 6, increased dissolved ( $\Sigma S \sim HS^- + S^{2-} \leq \!\! 35$  mg/l) and gaseous (H\_2S up to 8.7 vol.% in gas phase and odor of thermal water) sulfide concentrations, as well as relatively high chloride (up to 200 mg/l) and gaseous CO<sub>2</sub> (up to 90 vol.% of gas phase) contents. Next to these corrosive constituents, the high thermal fluid temperatures (reaching 141 °C in the aquifer) and high fluid discharges (up to 135 l/s) promote efficient and rapid steel corrosion. In the carbonate scales, we find no distinct evidence (e.g., dendritic filaments) of microbially influenced Fe corrosion and/or  $CaCO_3$  precipitation (Fan et al. 2013; Lanneluc et al. 2015) likely precluded by the hostile high fluid temperatures (Takai et al. 2008; Lerm et al. 2013). An origin of the sulfide layers from steel corrosion is further supported by the relatively low dissolved metal concentrations of the respective thermal waters (e.g., Fe  $\leq$  380 µg/l,



Cu  $\leq$ 2, Zn  $\leq$ 17, Ni  $\leq$ 26 µg/l; Seibt 2010). In contrast, aqueous silicic acid concentrations are relatively high (H<sub>4</sub>SiO<sub>4</sub> ~80 mg/l) supporting adsorption and co-precipitation of silica with the basal corrosion products (Figs. 2, 5) further promoted by cooling during thermal water ascent (decreasing solubility of silica). The hydrochemical data consequently suggest a principal origin from steel corrosion for the typically thin but variable metal sulfide layers within the carbonate scales (Fig. 4f; Additional file 1: Figure S1C). They could be the manifestation of flushing events in the course of restarts after major production cessations favoring sustained corrosion and detrital particle transport in suspension. Possibly, the particulate sulfide minerals are mobilized from deeper corroded pipe sections (below downhole pump) and/or from corroded steel surfaces of upper borehole sections accessible after some scale-fragment mobilization. However, some proportion of the metal sulfides detected could also originate from the anoxic aquifer, i.e., heavy metals mobilized from deep sediments as, e.g., Cl<sup>-</sup> or HS<sup>-</sup> aquo-complexes (Barnes 2015) and subsequently precipitated with the carbonate scale.

Calcite  $(CaCO_3)$  scale precipitation from the deep thermal waters and at the sulfide corrosion layers is represented by the overall reactions:

$$H_2CO_{3(aq)} = CO_{2(g)} + H_2O$$
 (2a)

$$HCO_3^- + H^+ = H_2CO_{3(aq)}$$
 (2b)

$$HCO_3^- = CO_3^{2-} + H^+$$
(2c)

$$Ca^{2+} + CO_3^{2-} = CaCO_{3(s)}$$
 (2d)

$$Ca^{2+} + 2HCO_3^- = CaCO_{3(s)} + H_2O + CO_{2(g)}.$$
 (2)

The chemical equilibria and finally  $CaCO_3$  mineralization in the aqueous carbonate system are mainly controlled by pressure-, temperature-, and pH (H<sup>+</sup> activity)-dependent dissolution and degassing of  $CO_2$  in the thermal waters, as well as calcium (and magnesium) and carbonate mobilization from the deep limestone/dolomite aguifer. Our results, however, also suggest a critical role of the underlying, corroded steel substrate. Abundant and competitive CaCO<sub>3</sub> crystallites at the scale versus corrosion mineral (metal sulfide) interface characterize an attractive substrate for initial nucleation and ongoing crystal growth (Figs. 4, 5). Such an enhancing effect is supported by the overall lower crystallinity, high specific surface areas, and common defect sites of typical corrosion mineral layers (Zimer et al. 2013; Bai et al. 2014). In this context, electrostatic forces could also play a role (Kashkovskiy et al. 2012; Fan et al. 2013). Regarding the overall progress of steel corrosion, the precipitation of carbonate and corrosion products might reduce the determining electrochemical reactions, i.e., reduce ongoing corrosion at places of significant scale deposition (cf. Nogara and Zarrouk 2014). Such an effect of scaling versus corrosion is also likely in the case presented here. Steel corrosion favoring initial calcite nucleation and thereby influencing further crystal growth, however, is in line with the observed extensive scaling progress in spite of relatively low total dissolved solid contents measured in the thermal waters ( $\leq$ 700 mg/l, Seibt 2010; Mayrhofer et al. 2014; Dussel et al. 2016). In addition, hydrochemical calculations (using PHREEQC)

reveal that calcite saturation states of thermal fluids sampled near the wellhead are close to equilibrium (only slightly supersaturated or even undersaturated). The calculated  $CO_2$  partial pressures are prominently high (log p $CO_2 = -0.9$  to -0.1 atm). It is important to note that the production wells of both geothermal facilities operate at a relatively high working pressure (~18 bar) in order to avoid outgassing. Several factors therefore counteract an increased calcite precipitation and support the potential role of some surficial trigger inducing the initiation of scale nucleation. Regarding the recurrent metal sulfide layers within the carbonate scales, such effects on crystallization may strongly depend on the local thickness of the attractive substrate (Fig. 4b; Additional file 1: Figure S1C), i.e., both continued (unperturbed) calcite growth or re-nucleation might occur.

## Scale-fragment development

Discussing scale formation and fragmentation, two interfaces are considered to be of crucial importance: (i) the interface between calcite scale and the sulfide corrosion products and (ii) the interface between thermal fluid and calcite scale. The metal sulfide corrosion products frequently evolving from the corrosion of carbon- and low-alloy steels interacting with H<sub>2</sub>S-rich thermal solutions possess distinct chemical and mechanical characteristics (Kashkovskiy et al. 2012; Zheng et al. 2015). Different sulfide corrosion mechanisms are distinguished, e.g., sulfide stress cracking (SSC; Bai et al. 2014; Liu et al. 2014) or pitting corrosion (Zimer et al. 2013; Nogara and Zarrouk 2014). In essence, these corrosion mechanisms result in localized but ongoing steel deterioration allowing corrosive constituents of the thermal fluid to further penetrate into the unaltered steel surface. This is also the case for hydrogen atoms and molecules emerging from sulfide corrosion [see chemical reactions (1)] and leading to widespread hydrogen-induced cracking (HIC) and hydrogen embrittlement favored at high temperatures (Liu et al. 2014; Bai et al. 2014). Increased H<sub>2</sub> gas concentrations also measured in the fluid flow of the geothermal facilities investigated in this study (Seibt 2010) are recognized as an indicator of significant corrosion (Smith et al. 2011; Alt-Epping et al. 2013). As a major consequence, steel surfaces become increasingly brittle and show a weakened mechanical resistance against (shearing) stress and strain, e.g., from the streaming thermal fluid. Macroscopic, microscopic, and high spatial resolution electron microprobe imaging support the common occurrence of small cracks and related flakes being closely associated with the corrosion product layers, i.e., (hairline) cracks are a common visible feature affecting the coherence of the sulfide corrosion layer and often also the adjacent calcite scale base (Figs. 4, 5).

Another prominent feature of the scale-fragments studied is their typically rough growth surface, i.e., the interface between thermal fluid flow and calcite scale. This was directly related to calcite nucleation, competitive and euhedral (rhombohedral) crystal growth determining the actual scale fabric. Importantly, a rough scale surface topography results in an increased flow resistance and higher frictional forces at the interface, probably causing the occurrence of (micro)turbulences. The latter would entail increased  $CO_2$  and  $H_2O$  outgassing from aqueous solution and such degassing would strongly enhance local supersaturation and further  $CaCO_3$  precipitation considering the respective chemical equilibria reported in the previous Eq. (2). High carbonate scale deposition rates and the resulting saturation states close to calcite equilibrium observed support

this mechanism. Moreover, the occurrence of (micro)turbulences at the interface can explain rapid calcite precipitation in spite of the typically high production well operating pressures ( $\sim$ 18 bar) applied in order to counteract outgassing. In this context, variable thermal water production rates will also affect the processes at the interface. The prominently high solution CO<sub>2</sub> partial pressures calculated further support a potential susceptibility with regard to a trigger of CO<sub>2</sub> degassing. Increased but variable degrees of CO<sub>2</sub> outgassing and steam (bubble) formation during thermal fluid flow are also strongly suggested by the analyzed C and O isotopic distribution and evolution in the carbonate scale-fragments (Fig. 6; Additional file 1: Tables S3, S4). The stable isotope measurements of the calcite precipitates show overall high  $\delta^{13}$ C values ranging from -1.5 to -0.5% (VPDB) primarily reflecting dissolution of the Malm aquifer limestone/dolomite and overall low  $\delta^{18}$ O values of -28.3 to -26.6‰ (VPDB) primarily reflecting the meteoric origin and high temperatures of the thermal waters. A comparison of the corresponding carbonate  $\delta^{13}$ C versus  $\delta^{18}$ O values does not show a significant correlation. The natural isotopic variability of deep thermal waters and consequently of carbonate formed over short time intervals (e.g., scale formation in this study) is typically considered to be very low. Micromilled (continuous) C and O isotope profiles show  $\delta^{13}$ C amplitudes of ~0.7‰ and  $\delta^{18}$ O amplitudes of ~1.5 and 1.3‰ for samples from KIR and DUR, respectively (Fig. 6). Importantly, these variations occur within short spatial (1-4 mm) and temporal (scaling rate >1 mm/month) intervals. Oxygen isotope fractionation between water and calcite is known to strongly depend on the prevailing temperature (Epstein et al. 1953; O'Neil et al. 1969). Based on published O isotope thermometers, it is possible to translate the measured calcite  $\delta^{18}$ O values (-28.1 to -26.6‰ VPDB for KIR33, Fig. 6, this study) and thermal water  $\delta^{18}$ O values (-11.7% VSMOW for KIR; Seibt 2010) into absolute temperature changes. Applying well-established fractionation factors, the lowest carbonate  $\delta^{18}$ O values (-28.1‰) result in calcite formation temperatures of (i) 136 °C (Friedman and O'Neil 1977) or (ii) 138 °C (Coplen 2007), i.e., reflecting the actual KIR thermal water temperatures in the production well between Malm aquifer (141 °C max.) and wellhead (134 °C typically) very well. In contrast, the higher carbonate  $\delta^{18}$ O values (-26.6‰) result in temperatures of (i) 118 °C (Friedman and O'Neil 1977) or (ii) 124 °C (Coplen 2007), i.e., much lower temperatures. Thus, relative water-temperature variations of (i) 18 °C or (ii) 14 °C should occur based on these calculations. This is not supported by typical ranges of temperature variations in these deep and high-discharge geothermal wells (few °C at wellhead). Consequently, temperature changes alone cannot explain the observed oxygen isotope fractionation. Rather, processes such as rapid CO<sub>2</sub> degassing and H<sub>2</sub>O vapor formation from solution are well known to kinetically enrich the isotopically light carbon dioxide  $({}^{12}C^{16}O_2)$  and water  $({}^{1}H_2^{16}O)$  molecules in the separated gas phase resulting in higher but variable  $\delta^{13}$ C versus  $\delta^{18}$ O values of the precipitating calcite (Mickler et al. 2006; Dreybrodt and Romanov 2016). These processes of kinetic isotope fractionation vary temporally and spatially depending on the amount and proportion of partial gas separation of  $CO_2$  and  $H_2O$ . Altogether, we interpret the distinct isotope variations analyzed in the scales to primarily reflect physicochemical processes such as variable CO<sub>2</sub> and H<sub>2</sub>O (steam) outgassing, a variable degree of (micro) turbulences in the pipes, some contribution from temperature changes and minor natural isotopic variability. These combined effects are further closely linked to production



rate and thus operational conditions, which can be monitored temporally and spatially by the above stable isotope signatures of the calcite considering a small impact by natural isotope variations. Importantly, the amount of carbonate scale deposition (scaling progress) is intimately connected with the variable release of  $CO_2$  and  $H_2O$  from the streaming thermal water [see chemical equilibria reported in Eq. (2)].

Regarding a conceptual understanding of scale-fragment development, the partial exfoliation within the vertical or horizontal transport pipes strongly relies on the preconditions at the two interfaces discussed (Fig. 7). Mobilization is favored by (i) the



chemically and mechanically weak basal (sulfide) corrosion interface and (ii) increased flow resistance and associated (micro)turbulences at the rough calcite scale growth surface. In addition, flaking off might be promoted by some thermal contraction, e.g., from cooling of steel pipes during major production cessations. Also, additional mechanical stress on the rough scale surface could result from particle transport in suspension and abrasion. Significantly increased particle concentrations were observed during restart procedures after production cessations (Wolfgramm et al. 2011). After mobilization within thermal water flow (up to 135 l/s), the scale-fragments impact and eventually damage the relatively fragile outer surfaces of the pounded heat exchangers. Finally, severe clogging of heat exchangers or filters (obstacles) is accomplished by successive accumulation, agglomeration, and CaCO<sub>3</sub> cementation during ongoing but deteriorating thermal fluid flow and heat/energy extraction (Fig. 7).

## Conclusions and environmental and technical considerations

Our scaling forensic approach highlights the critical interaction of natural and technical (operational) conditions with regard to an increased carbonate scaling and steel corrosion potential and associated problematic scale-fragment development. The exploitation of Upper Jurassic carbonate aquifer H<sub>2</sub>S-containing Na-Ca-HCO<sub>3</sub>-Cl thermal water (Mayrhofer et al. 2014; Stober 2014; Dussel et al. 2016; Goldbrunner and Vasvari 2016) entails a significant hydrogeochemical potential for both carbonate scaling and steel corrosion. This natural environmental potential consists in the initial versus disturbed dissolved carbonate equilibria leading to carbonate scaling and several corrosive constituents ( $H_2S$ ,  $CO_2$ ,  $CI^-$ ,  $H_2$ ) in combination with high temperatures and high flow rates (component supply) effecting steel deterioration. Evaluating the source of H<sub>2</sub>S delivered with the regional thermal waters, thermochemical sulfate reduction (TSR) at sufficiently high temperatures (100-140 °C) and in association with various organic materials was discussed (Mayrhofer et al. 2014). These redox reactions would also contribute to the dissolved (inorganic) carbon budget, although the high aqueous solution  $(\delta^{13}C_{DIC}=-0.2\%$  VPDB; Seibt 2010) and high calcite scale ( $\delta^{13}C=-1.5$  to -0.5%VPDB; this study) stable carbon isotopic compositions argue against a major organic contribution with regard to dissolved carbonate species and potential carbonate precipitation. Based on the available hydrochemical data and calculations performed, it further seems possible that the scaling problems encountered at the study sites are partially the result of physicochemical conditions associated with a deep fault zone. This is supported by prominently high aqueous solution pCO<sub>2</sub> values, high water temperatures, and eventually other (e.g., sulfur isotopic) indicators. Fault zones are considered a primary target of productive geothermal wells in the region although being difficult to constrain spatially (Wolfgramm et al. 2009; Stober 2014; Dussel et al. 2016; Goldbrunner and Vasvari 2016, Przybycin et al. 2017). Deep faults delivering abundant  $CO_2$  might further be associated with hypogenic karstification, i.e., providing an efficient mechanism for aquifer host rock dissolution and potential secondary carbonate precipitation. In essence, fault zones could entail favorable (high discharge and high temperature) as well as unfavorable (chemical constituents such as CO<sub>2</sub>) production conditions. Considering the technical (operational) potential of the two studied geothermal doublets with regard to carbonate scaling and corrosion in the production wells, the selection of materials in contact with the thermal fluid is likely of major importance. The occurrence of metal sulfide corrosion layers favoring scale-fragment development and probably being a partial source of the dark scale coloring should diminish when more corrosion resistant (alloyed or coated surface) steels are used. A major effect of corrosion layers enhancing carbonate precipitation in contrast to plastic coatings reducing the overall scale thicknesses was supported by observations and simulations of a recent study (Wanner et al. 2017). We are aware, however, that the application of specific materials might not always be viable due to other circumstances (e.g., costs, abrasive effects, temperature resistance). In order to avoid accumulation and critical cementation of scale-fragments, these should be filtered/removed timely and near the heat exchanger surface or other obstacles during water flow. Thermal water production cessations and restarts most likely have a significant effect on scale-fragment mobilization, i.e., causing additional mechanical stress from pressure and temperature changes, increased (micro)turbulences, and probably elevated (abrasive) particle concentrations. To summarize, scaling forensics can help to better understand the site-specific favorable and unfavorable physicochemical processes determining scaling and/or corrosion of affected geothermal power plants.

### **Additional file**

Additional file 1. Additional figures and tables.

#### Authors' contributions

The manuscript was written through contributions of all authors. All authors read and approved the final manuscript.

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#### **Competing interests**

The authors declare that they have no competing interests.

#### Availability of data and materials

The datasets supporting the conclusions of this article are included within the article and its additional information. Figures of additional microscopic characterization of scale-fragment fabrics based on reflected and transmitted light and electron microscopy; Tables of minor and trace elemental compositions of the mineral precipitates based on XRF, ICP-OES, and ICP-MS analysis; and stable carbon and oxygen isotopic compositions of selected micromilled and drilled carbonate scales are provided.

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